

Derivation of Pressure Profile in Steady-State Homogeneous Pipe Flow @model

The base driving equations of a pipe flow are:

Steady-state 1D inviscid fluid flow	Pipe Flow Mass Conservation
(1) $\frac{dp}{dl} = -\rho u \frac{du}{dl} + \rho g \cos \theta + f_{\text{cnt},l}$	(2) $j_m(l) = j_m = \rho(l) \cdot u = \text{const}$
Equation of State (EOS)	
(3) $\rho = \rho(p, T)$	(4) $f_{\text{cnt},l} = -f \cdot \frac{\rho u^2}{2d}$

where

l	distance along the fluid flow streamline
$\theta(l)$	inclinational deviation, $\cos \theta = dz/dl$
$z(l)$	elevation along the 1D flow trajectory
$T(l)$	fluid temperature
$p(l)$	fluid pressure
$\rho(l)$	fluid density
$\mathbf{u}(l)$	fluid velocity vector
$u(l)$	superficial velocity of the pipe flow
$\mathbf{f}_{\text{cnt}}(l)$	volumetric density of all contact forces exerted on fluid body
$f_{\text{cnt},l}(l) = \mathbf{e}_u \cdot \mathbf{f}_{\text{cnt}}$	projection of \mathbf{f}_{cnt} onto the unit fluid velocity vector: $\mathbf{e}_u = \mathbf{u} ^{-1} \mathbf{u}$
$j_m = \rho(l) \cdot u(l)$	fluid mass flux
\dot{m}	mass flowrate
g	standard gravity constant

Substituting (2) and (4) into (1):

$$(5) \quad \frac{dp}{dl} = -j_m \cdot \frac{d}{dl} \left(\frac{j_m}{\rho} \right) + \rho g \cos \theta - f \cdot \frac{\rho}{2d} \cdot \left(\frac{j_m}{\rho} \right)^2$$

$$(6) \quad \frac{dp}{dl} = j_m^2 \cdot \frac{1}{\rho^2} \frac{d\rho}{dl} + \rho g \cos \theta - \frac{j_m^2}{2d} \cdot \frac{f}{\rho}$$

$$(7) \quad \frac{dp}{dl} = j_m^2 \cdot \frac{1}{\rho^2} \frac{d\rho}{dl} \cdot \frac{dp}{dl} + \rho g \cos \theta - \frac{j_m^2}{2d} \cdot \frac{f}{\rho}$$

$$(8) \quad \frac{dp}{dl} = j_m^2 \cdot \frac{1}{\rho} \cdot c \cdot \frac{dp}{dl} + \rho g \cos \theta - \frac{j_m^2}{2d} \cdot \frac{f}{\rho}$$

and finally

$$(9) \quad \left(1 - j_m^2 \cdot \frac{c}{\rho} \right) \frac{dp}{dl} = \rho g \cos \theta - \frac{j_m^2}{2d} \cdot \frac{f}{\rho}$$

Alternative forms

$$(10) \quad [\rho - j_m^2 c] \cdot \frac{dp}{dl} = \rho^2 g \cos \theta - \frac{j_m^2}{2d} \cdot f(\rho)$$

$$(11) \quad \left[\frac{1}{c} - \frac{j_m^2}{\rho} \right] \cdot \frac{dp}{dl} = \rho^2 g \cos \theta - \frac{j_m^2}{2d} \cdot f(\rho)$$

See Also

[Petroleum Industry / Upstream / Pipe Flow Simulation / Water Pipe Flow @model](#) / [Stationary Isothermal Homogenous Pipe Flow Pressure Profile @model](#)

[[Darcy friction factor](#)] [[Darcy friction factor @model](#)]

[[Euler equation](#)]