

# Temperature Profile in Homogenous Stationary Pipe Flow

## Analytical Ramey @model

### Motivation

Analytical model of temperature step-response in a Homogenous Stationary Pipe Flow with account for the heat exchange with surroundings

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Model equally works for wellbore flow, ground, on-ground and bottom-water pipelines.

### Outputs

$T(t, l)$  Along-hole Temperature Profile

where

$t$	Flowing duration
$l$	Length along pipe

### Inputs

$T_s$	Intake temperature	$T_e(l)$	Background temperature of the surroundings
$\dot{m}$	Mass flowrate	$U$	Heat Transfer Coefficient (HTC) between pipe fluid and surroundings
$a_e$	Thermal Diffusivity of the surroundings	$r_f$	Flowing pipe radius
$\lambda_e$	Thermal Conductivity of the surroundings	$r_w$	Wellbore radius

### Equations

(1) $T(t, l) = T_e(l) - R(t) G_e(l) + [T_s - T_e(0) + R(t) G_e(l)] \cdot e^{-l/R(t)}$	(2) $G_e = \frac{dT_e}{dl}$	(3) $t_D(t) = \frac{a_e t}{r_w^2}$
(4) $R(t) = \frac{\dot{m} c_p}{2\pi \lambda_e} \cdot \left( T_D(t) + \frac{\lambda_e}{r_f U} \right)$	(5) $T_D(t) = \ln \left[ e^{-0.2 t_D} + (1.5 - 0.3719 e^{-t_D}) \sqrt{t_D} \right]$	

### Assumptions

Intake Flowrate is constant in time

Intake Temperature is constant in time

$q_s(t) = q_s = \text{const}$	$T_s(t) = T_s = \text{const}$
<b>Thermal diffusivity of the surroundings is constant along-hole</b>	<b>Thermal Conductivity of the surroundings is constant along-hole</b>
$a_e(l) = a_e = \text{const}$	$\lambda_e(l) = \lambda_e = \text{const}$
<b>Flowing pipe radius is constant along-hole</b>	<b>Wellbore radius is constant along-hole</b>
$r_f(l) = r_f = \text{const}$	$r_w(l) = r_w = \text{const}$
<b>Heat Transfer Coefficient (HTC) between pipe fluid and surroundings is constant along-hole</b>	
$U(l) = U = \text{const}$	

## See Also

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[Physics](#) / [Fluid Dynamics](#) / [Pipe Flow Dynamics](#) / [Pipe Flow Simulation](#) / [Temperature Profile in Pipe Flow @model](#) / [Temperature Profile in Homogenous Pipe Flow @model](#)

## References

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