

# Temperature Profile in Homogenous Stationary Pipe Flow

## @model

### Motivation

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One of the key challenges in [Pipe Flow Dynamics](#) is to predict the along-hole [temperature](#) distribution during the [stationary fluid transport](#).

[Pipeline Flow Temperature Model](#) is addressing this problem with account of the varying [pipeline trajectory](#), [pipeline schematic](#) and [heat transfer](#) with the matter around [pipeline](#).

In many practical cases the along-hole [temperature](#) distribution during the [stationary fluid flow](#) can be approximated by [homogenous fluid flow](#) model.

### Outputs

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|           |   |
|-----------|---|
| $T(t, l)$ | along-pipe <a href="#">temperature</a> distribution and evolution in time |
|-----------|---|

### Inputs

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|                 |   |                |  |
|-----------------|---|----------------|--|
| $\mathbf{r}(l)$ | <a href="#">pipeline trajectory</a> , $\mathbf{r}(l) = \{x(l), y(l), z(l)\}$          | $\rho(T, p)$   | <a href="#">fluid density</a>  |
| $A(l)$          | <a href="#">pipeline cross-section area</a>   | $\mu(T, p)$    | <a href="#">fluid viscosity</a>  |
| $T_0(t)$        | intake temperature  | $T_{e0}(l)$    | initial temperature of the medium around the <a href="#">pipeline</a>                |
| $p_0$           | intake pressure   | $c_p(l)$       | <a href="#">specific heat capacity</a> of the medium around <a href="#">pipeline</a> |
| $q_0$           | intake flowrate   | $\lambda_e(l)$ | <a href="#">thermal conductivity</a> of the medium around <a href="#">pipeline</a>   |
| $U(l)$          | <a href="#">heat transfer coefficient</a> based on <a href="#">pipeline schematic</a> |                |  |

### Assumptions

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|-----------------------|--------------------------------|-----------------------|
| Stationary fluid flow | Axial symmetry around the pipe | Homogenous fluid flow |
|-----------------------|--------------------------------|-----------------------|

### Equations

|  |   |
|--|---|
| (1) $\rho c \frac{\partial T}{\partial t} = \frac{d}{dl} \left( \lambda \frac{dT}{dl} \right) - \rho c v \frac{dT}{dl} + \frac{U}{r_w} \cdot (T_e(t, l, r_w) - T)$ | (2) $\rho_e c_e \frac{\partial T_e}{\partial t} = \nabla(\lambda_e \nabla T_e)$ |
| (3) $T(t = 0, l) = T_{e0}(l)$  | (4) $T_e(t = 0, l, r) = T_{e0}(l)$  |
| (5) $T(t, l = 0) = T_0(t)$   | (6) $T_e(t, l, r \rightarrow \infty) = T_{e0}(l)$                               |
| (7) $2\pi \lambda_e r_w \frac{\partial T_e}{\partial r} \Big _{r=r_w} = 2\pi r_f U \cdot \left( T_e \Big _{r=r_w} - T \right)$                                     |   |

## Approximations

Temperature Profile in Homogenous Stationary Pipe Flow Analytical Ramey @model

## See also

[Physics / Fluid Dynamics / Pipe Flow Dynamics / Pipe Flow Simulation / Temperature Profile in Pipe Flow @model](#)

[ [Heat Transfer](#) ][ [Heat Transfer Coefficient \(HTC\)](#) ]

[ [Stationary Isothermal Homogenous Pipe Flow Pressure Profile @model](#) ][ [Pipe Flow Temperature Analytical Ramey @model](#) ]

## References

[https://en.wikipedia.org/wiki/Darcy\\_friction\\_factor\\_formulae](https://en.wikipedia.org/wiki/Darcy_friction_factor_formulae)

[https://neutrium.net/fluid\\_flow/pressure-loss-in-pipe/](https://neutrium.net/fluid_flow/pressure-loss-in-pipe/)

